

Application of New Models in Rheological Behavior Study Sunflower Oil

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Author's contribution

This work was done by the author IS designed the study, the statistical analysis performed, wrote the protocol, and wrote the first draft of the manuscript, managed the analyses of the study, managed the literature researches and read and approved the final manuscript.

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ABSTRACT

Sunflower oil is the non-volatile oil compressed from sunflower (*Helianthus annuus*) seeds. Sunflower oil contains predominantly linoleic (48–7%), oleic (14–40%), palmitic (4–9%) and stearic (1–7%). In general, viscosity measures the resistance of a liquid to flow. From a molecular point of view, viscosity is an indirect measurement of the internal friction between the molecules that constitute the fluid and which oppose liquid movement. Therefore, viscosity must have significant correlations with structural parameters of the fluid molecules.

The sunflower oil were investigated using a Haake VT 550 Viscotester developing shear rates ranging between 3 and 120 s⁻¹ and measuring viscosities from 10⁴ to 10⁶ mPa.s when the HV₁ viscosity sensor is used. In this article we presented rheological models to study the behavior of sunflower oil. The constants A, B, and C were determined by Origin 6.0 software by fitting exponential curves obtained from experimental data. The one proposed relationship gives correlation coefficients close to one. For three-dimensional representation of the shear rate by shear stress at different temperatures we used Origin 6.0 software. From the diagram it is observed that at low temperatures sunflower oil has the highest shear stress and therefore dynamic viscosity highest at high temperatures sunflower oil has the lowest shear stresses and therefore dynamic viscosity lowest.

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1. INTRODUCTION

Sunflower oil is the non-volatile oil compressed from sunflower (*Helianthus annuus*) seeds. Sunflower oil contains predominantly linoleic (48–7%), oleic (14–40%), palmitic (4–9%) and stearic (1–7%) [1-4].

In general, viscosity measures the resistance of a liquid to flow. From a molecular point of view, viscosity is an indirect measurement of the internal friction between the molecules that constitute the fluid and which oppose liquid movement. Therefore, viscosity must have significant correlations with structural parameters of the fluid molecules [5-9].

The viscosity of sunflower oil decreases logarithmically with temperature, but the slope representing the change is lessened. Different equations are proposed in literature to calculate the shear stress [10-14].

Bingham:

$$\tau = \tau_0 + \eta \dot{\gamma} \quad (1)$$

Casson:

$$\tau^{1/2} = \tau_0^{1/2} + \eta^{1/2} \dot{\gamma}^{1/2} \quad (2)$$

Ostwald-de Waele:

$$\tau = k \dot{\gamma}^n \quad (3)$$

and Herschel-Bulkley:

$$\tau = \tau_0 + k \dot{\gamma}^n \quad (4)$$

where τ is the shear stress, τ_0 – yield stress, η - viscosity, $\dot{\gamma}$ - shear rate, n – flow index and k – index of consistency.

This article proposes new models in rheological behavior study sunflower oil.

2. MATERIALS AND METHODS

The sunflower oil used in this work is provided by a company from Bucharest, Romania. The sunflower oil were investigated using a Haake VT 550 Viscotester developing shear rates ranging between 3 and 120 s⁻¹ and measuring viscosities from 10⁴ to 10⁶ mPa.s when the HV₁ viscosity sensor is used. The temperature ranging was from 40 to 100°C and the measurements were made from 10 to 10 degrees. The accuracy of the temperatures was ± 0.1°C.

3. RESULTS AND DISCUSSION

The rheograms of sunflower oil obtained from experimental data at the specified temperatures and shear rates are shown in Fig. 1(B), 2(C), 3(D), 4(E), 5(F), 6(G) and 7(H). Parameter values are given inside the Fig. 1, the correlation coefficient is 0.99991 at 40°C for sunflower oil. The exponential dependence of shear stress on the shear rate for sunflower oil at 40° C is described for equation (5):

$$\tau = (-2.12556E7) + 2.12556E7 \exp\left[\frac{\dot{\gamma}}{-1.07257E6}\right] \quad (5)$$

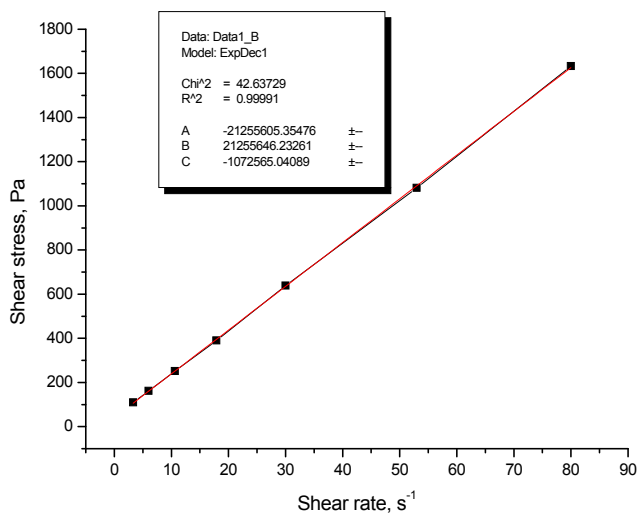


Fig. 1. Rheograms of sunflower oil at 40°C and 1B represent the fitting exponential to B

The values are: A = -2.12556E7, B = 2.12556E7 and C = -1.07257E6. At a temperature 40° C measurement errors were 42.63729.

The sunflower oil shows an exponential shear stress with shear rate as shown in Fig. 2. Parameter values are given inside the figure, the correlation coefficient is 0.9997 at 50° C sunflower oil. The exponential dependence of shear stress on the shear rate for sunflower oil at 50° C is described for equation (6):

$$\tau = 88606.96966 - 88566.71219 \exp\left(-\frac{\dot{\gamma}}{8627.17304}\right) \quad (6)$$

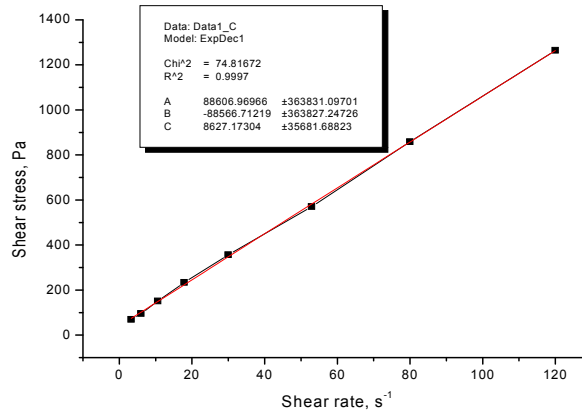


Fig. 2. Rheograms of sunflower oil at 50°C and 1C represent the fitting exponential to C

At temperature 50°C the parameter A increased by -21344206.96966 units, the parameter B has decreased by 21167033.2879 units and the parameter C increased by -1081127.17304 units. Increasing the temperature by 10°C leads to a higher error 32.17943 units.

The sunflower oil shows an exponential shear stress with shear rate as shown in Fig. 3. Parameter values are given inside the figure, the correlation coefficient is 0.99972 at 60°C sunflower oil. The exponential dependence of shear stress on the shear rate for sunflower oil at 60°C is described for equation (7):

$$\tau = 9459.11533 - 9428.57558 \exp(-\dot{\gamma} / 921.91261) \tag{7}$$

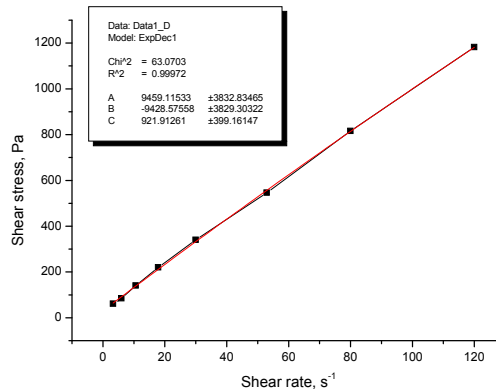


Fig. 3. Rheograms of sunflower oil at 60°C and 1D represent the fitting exponential to D

Increasing the temperature by 20°C the parameter A increased by -21265059.11533 units, the parameter B has decreased by 21246171.42442 units and the parameter C increased by -1073491.91261 units. At 60°C measurement error increases with 20.4326 units.

The sunflower oil shows an exponential shear stress with shear rate as shown in Fig. 4. Parameter values are given inside the figure, the correlation coefficient is 0.99981 at 70°C

sunflower oil. The exponential dependence of shear stress on the shear rate for sunflower oil at 70°C is described for equation (8):

$$\tau = 5055.54009 - 5031.03084 \exp(-\dot{\gamma} / 499.19029) \quad (8)$$

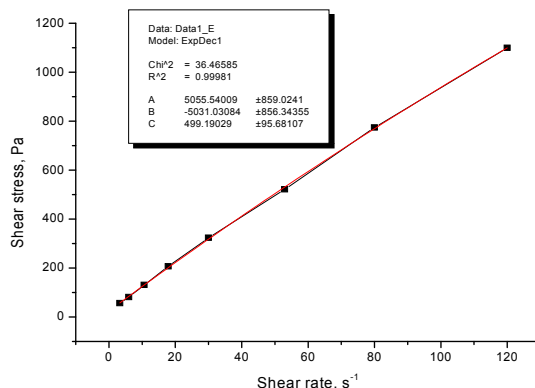


Fig. 4. Rheograms of sunflower oil at 70°C and 1E represent the fitting exponential to E

Increasing the temperature by 30°C the parameter A increased by -21260655.54009 units, the parameter B has decreased by 21250568.96916 units and the parameter C increased by -1073069.19029 units. At 70° C measurement error decreases with 5.97879 units.

The sunflower oil shows an exponential shear stress with shear rate as shown in Fig. 5. Parameter values are given inside the figure, the correlation coefficient is 0.99986 at 80°C sunflower oil. The exponential dependence of shear stress on the shear rate for sunflower oil at 80°C is described for equation (9):

$$\tau = 3581.15799 - 3561.71378 \exp(-\dot{\gamma} / 361.87488) \quad (9)$$

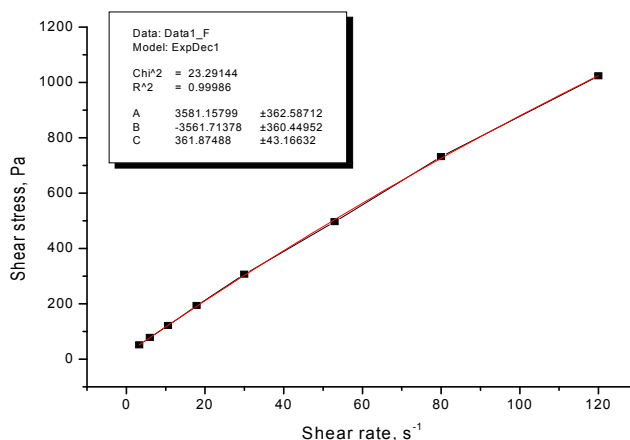


Fig. 5. Rheograms of sunflower oil at 80°C and 1F represent the fitting exponential to F

Increasing the temperature by 40° C the parameter A increased by -21259181.15799 units, the parameter B has decreased by 21252038.28622 units and the parameter C increased by -1072931.87488 units. At 80° C measurement error decreases with 19.34585 units.

The sunflower oil shows an exponential shear stress with shear rate as shown in Fig. 6. Parameter values are given inside the figure, the correlation coefficient is 0.99983 at 90°C sunflower oil. The exponential dependence of shear stress on the shear rate for sunflower oil at 90° C is described for equation (10):

$$\tau = 3156.74537 - 3135.52088 \exp(-\dot{\gamma} / 343.68052) \quad (10)$$

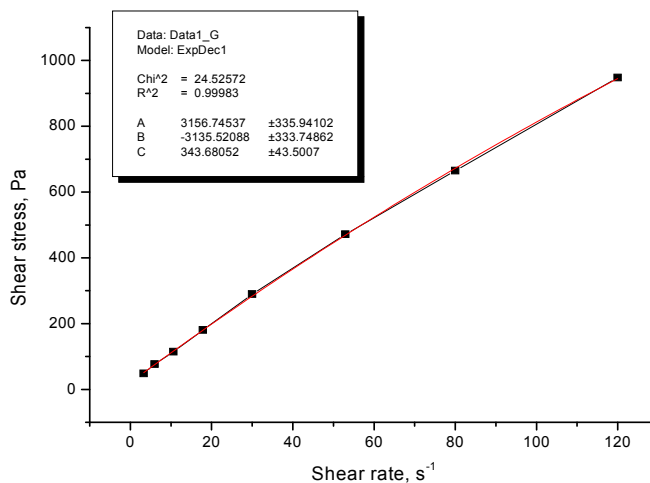


Fig. 6. Rheograms of sunflower oil at 90°C and 1G represent the fitting exponential to G

Increasing the temperature by 50° C the parameter A increased by -21258756.74537 units, the parameter B has decreased by 21252464.47912 units and the parameter C increased by -1072913.68052 units. At 90° C measurement error decreases with 18.11157 units.

The sunflower oil shows an exponential shear stress with shear rate as shown in Fig. 7. Parameter values are given inside the figure, the correlation coefficient is 0.99992 at 100°C sunflower oil. The exponential dependence of shear stress on the shear rate for sunflower oil at 100° C is described for equation (11):

$$\tau = 5337.67775 - 5314.09081 \exp(-\dot{\gamma} / 639.8184) \quad (11)$$

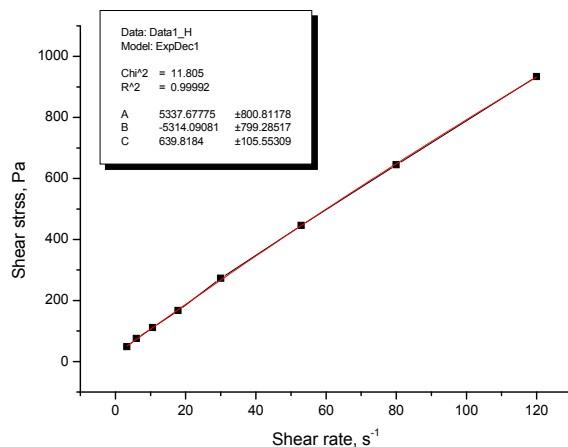


Fig. 7. Rheograms of sunflower oil at 100°C and 1H represent the fitting exponential to H

Increasing the temperature by 60°C the parameter A increased by -21260937.67775 units, the parameter B has decreased by 21250285.90919 units and the parameter C increased by -1073209.8184 units. At 100°C measurement error decreases with 30.83229 units.

Fig. 8 shows rheograms sunflower oil in three-dimensional presentation. For three-dimensional representation of the shear rate by shear stress at different temperatures we used Origin 6.0 software. From this diagram is can observe that with the temperature increasing the shear stress of sunflower oil decrease at each constant shear rate. This diagram shows that the viscosity of sunflower oil is correlated with the shear rate at a given temperature and negatively correlated to the temperature at constant shear rate. If sunflower oil is used as raw material in industry, high temperatures will not affect the rheological characteristics at 80° C and 90°C.

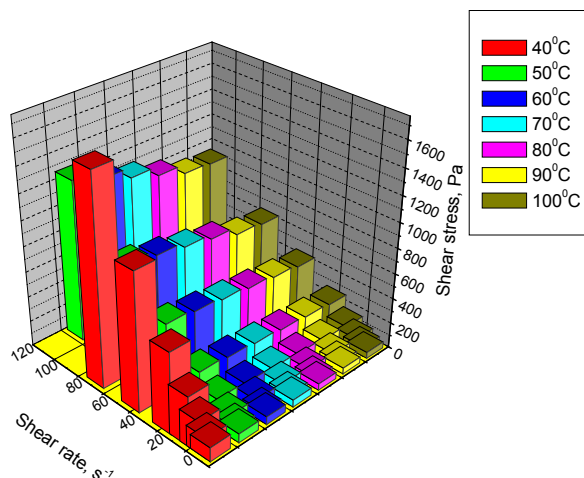


Fig. 8. Rheograms for sunflower oil at all temperatures

4. CONCLUSION

The dynamic viscosity of sunflower oil was determined at temperatures between 313 and 373K and shear between $3.3s^{-1}$ and $120s^{-1}$. This article proposes new models in rheological behavior study sunflower oil. The values of constants A, B and C and the correlation coefficients were determined by exponential fitting of the experimental curves using Origin 6.0 software.

COMPETING INTERESTS

Author has declared that no competing interests exist.

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